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Cathodic protection: A general discussion of the involved processes and their consequences for threshold values

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Korrosionsschutz ablaufenden Prozesse erforderlich. Die im Rahmen der Untersuchungen ermittelten grundsätzlichen Konzepte für den Mechanismus des kathodischen Korrosionsschutzes und deren Konsequenzen auf die Grenzbedingungen diskutiert.

Résumé

La protection cathodique a augmenté la durabilité des conduites. Les limites utilitaires de la protection cathodique sont éprouvées. Malheureusement sous courant constant ou alternatif ils ne sont plus applicables. Pour l'évaluation des limites de protection cathodique, la compréhension des mécanismes de corrosion est nécessaire. Ces concepts fondamentaux, leur pertinence et leur conséquence pour les limites est discutée.

It turned out that under a.c. interference a high cathodic protection current leads to detrimental effects on the durability of cathodically protected structures. These surprising observations in the case of a.c. and d.c. interference demonstrate that a profound understanding of the processes taking place on the steel surface is required. When the involved mechanisms are understood, the determination of parameter-related thresholds is possible.

Experimental

For all electrochemical characterizations and potential measurements a Jaissle PCT 1002 Galvanostat PCT 1002 in combination with a computer was used. The Coupons with a surface of 1 cm^2 were used for all tests. Solutions were prepared from reagent grade chemicals and de-ionized water. The electrolytes used in this work were borate buffer with a pH-value of 8.4 ($0.075 \text{ M Na}_2\text{B}_4\text{O}_7 \cdot 10 \text{ H}_2\text{O}$, $0.3 \text{ M H}_3\text{BO}_3$), $0.1 \text{ M Na}_2\text{SO}_4$, 0.01 M NaOH . All potentials are referred to saturated Copper/Copper sulfate electrode.

presence of the oxidizing agent oxygen in the electrolyte. In the case of copper protection can be achieved by shifting the potential from the corrosion range of diagram (Fig. 1) to the immunity range.

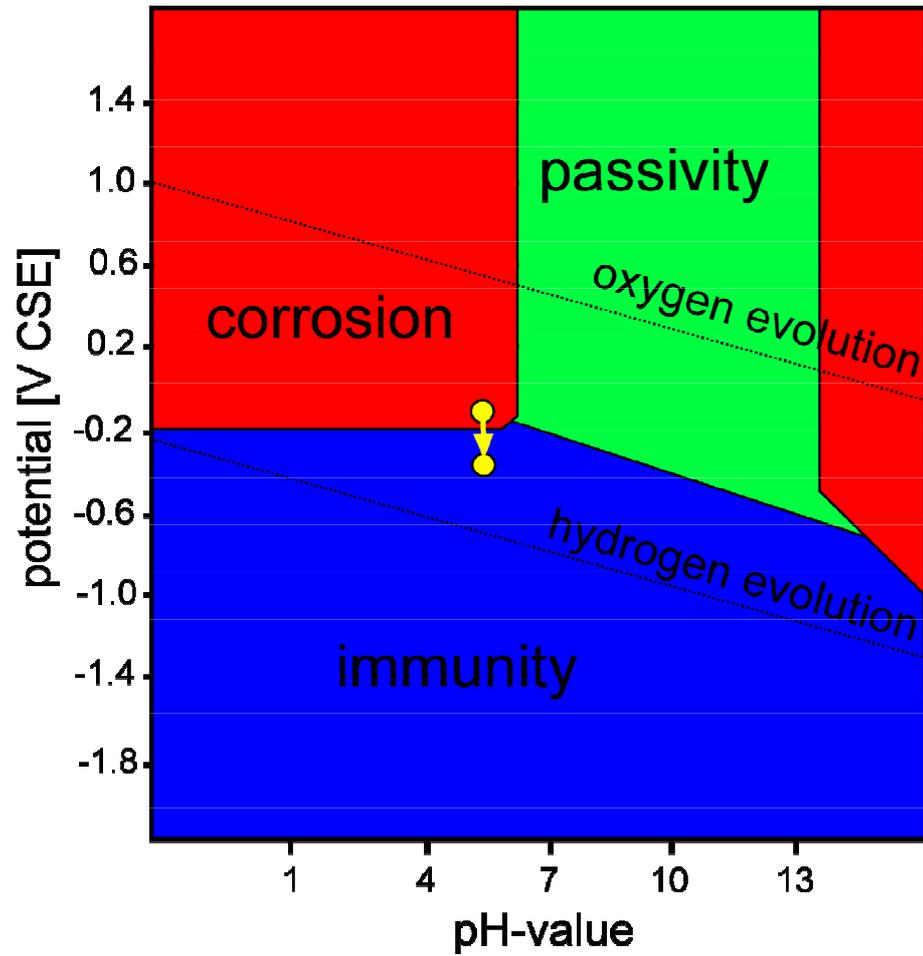


Fig. 1: Pourbaix diagram for copper. Shift of the potential from the corrosion to range by the cathodic protection current.

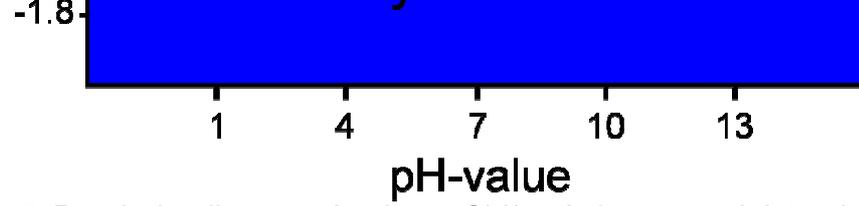


Fig. 2: Pourbaix diagram for iron. Shift of the potential to the hydrogen evolution reaction at high pH values due to cathodic protection current.

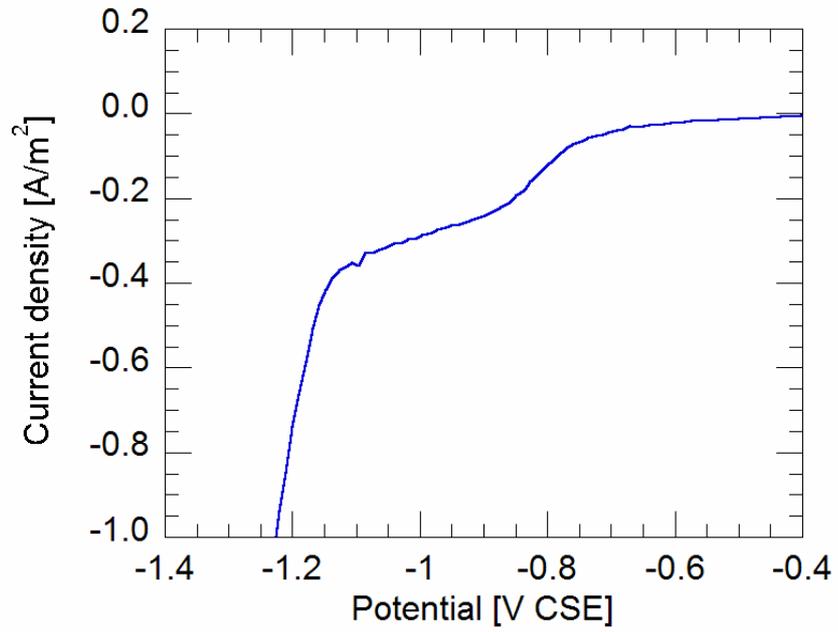


Fig. 3: Cathodic polarization scan of steel in 0.1 M NaOH with pH 13.

In Fig. 2 the Pourbaix diagram for iron is shown. It is important to note that the potential for the oxidation reaction (3), which is the transition from immunity to

27). In this range the formation of a protective passive film is thermodynamically favorable. When reaching the field of passivity the potential of the steel surface gets below -0.85 V CSE, which is the threshold value for the off potential. Since this value is not in the range, the question arises regarding the protection mechanism. Clearly, the mechanism is different compared to the situation described for copper. There are several factors that contribute to the corrosion protection of steel:

- Corrosion is only possible when the electrons formed in reaction (3) are consumed. The predominant reducing agent is oxygen. Hence the depletion of oxygen from the steel surface results in a decrease in the corrosion rate.
- The reduction reactions taking place on the steel surface increase the pH of the electrolyte. If the pH is sufficiently high, the steel surface is covered by a protective passive film that strongly decreases the corrosion rate.
- The lowering of the potential of the steel surface decreases the driving force for reaction (3). Therefore, the corrosion rate is decreased. Moreover, the galvanic couples due to aeration elements along the pipeline are eliminated.

As a consequence, the positive effect of cathodic protection is caused by the combination of all three effects. Based on the discussion of the processes taking place during cathodic protection, a potential below -0.85 V CSE can only be reached when the oxygen is depleted and the alkalinity is sufficiently high to allow the formation of a protective passive film. As a consequence, the measurement of the off potential effectively is a combination of oxygen and pH measurement. This is illustrated by the potential measurements in electrolytes with different pH values (Fig. 4). The oxygen content of these electrolytes is decreased by purging with nitrogen. Clearly the potential decreases rapidly when the oxygen content is lowered. In the case of the electrolyte with pH 12 the potential drops below -0.85 V CSE after a few minutes. This effect is even more pronounced at pH 14, where in the solution the potential does not drop below -0.73 V CSE. This experiment confirms the theoretical conclusions.

Corrosion due to a.c. interference

Now that the mechanism of the cathodic protection and the significance of the current density value are discussed the question arises regarding their consequences for cathodic protection under a.c. interference. The involved mechanisms are described in detail in [4]. In Fig. 5 the corrosion mechanism is illustrated. The repeated complete formation and destruction of the passive film results in a corrosion rate of up to 70 mm/year and in the formation of a thick rust layer.

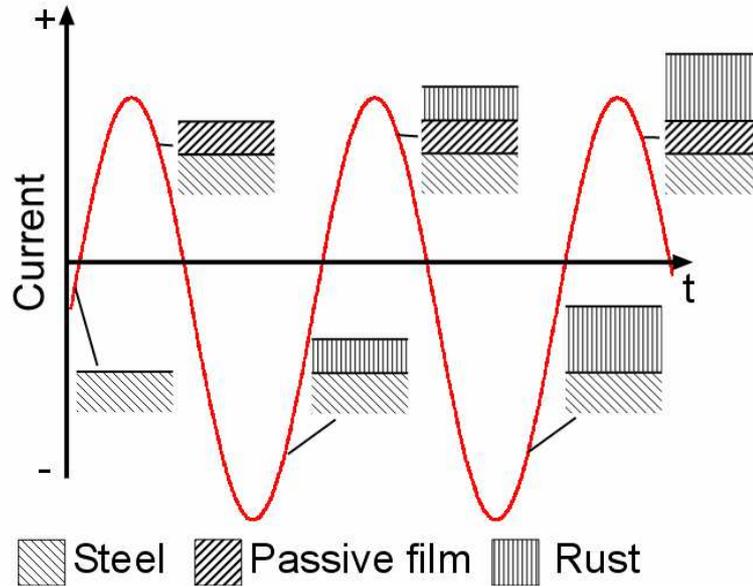


Fig. 5: Mechanism of a.c. corrosion.

This corrosion process can be stopped if the once formed passive film is not destroyed anymore. This is achieved by decreasing the cathodic protection current. It is important to note that a certain rust layer thickness is required for the consumption of the cathodic charge of the a.c. current by reaction (5). In an extended field and laboratory tests the relevant threshold values were experimentally determined [6]. It was demonstrated that the corrosion rate remains acceptable if the average on potential is more positive than the threshold value.

$$I_{d.c.} = \frac{E_{on} - E_{off}}{R}$$

In order to explain the experimentally observed threshold value of -1.2 V CSE potential, the effects taking place during cathodic protection have to be considered in the Pourbaix diagram (Fig. 6). As soon as the hydrogen evolution takes place on the surface, the off potential is shifted along the equilibrium line for hydrogen evolution. In Fig. 6 it becomes clear that there is an intersection between the line for hydrogen evolution and the line for an E_{on} of -1.2 V CSE. As a consequence, the difference between E_{on} and E_{off} according to equation (1) will go towards zero for high pH values, limiting the d.c. current density. This will limit the increase of surface pH and, therefore, equilibrium will be established preventing an uncontrolled increase of the d.c. current density. In case of an E_{on} of -1.3 V CSE the driving voltage can only go towards zero at unrealistic high pH values and, therefore, the d.c. current density can strongly increase and cause a.c. corrosion. It is important to note that the field of corrosion at high pH cannot be the primary cause of a.c. corrosion, since on potentials more negative than -1.2 V CSE in absence of a.c. current density do not cause any corrosion.

Based on this discussion the question arises regarding the negative effect of the a.c. current density on the off potential. In previous investigations it was demonstrated that the a.c. current density causes a shift of the E_{off} to positive values [5]. This so called faradaic rectification is caused by the asymmetry of the polarization curves (e.g. Fig. 3). This rectification becomes significant at a.c. current densities above 30 A/m² explaining the significance of this threshold value. A shift of the E_{off} to more positive values will additionally increase the d.c. current density according to equation (1) and therefore cause a.c. corrosion. Based on this discussion the negative effect of the a.c. current density in the case of low cathodic protection is primarily the increase of the d.c. current density.

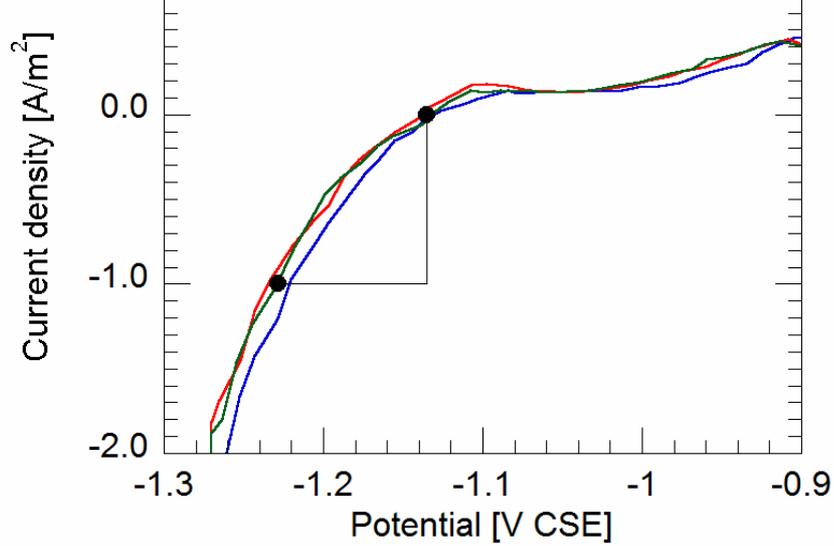


Fig. 7: Anodic polarisation scans of steel in 0.1 M NaOH (pH 13). The potential shift associated with a cathodic current of 1 A/m² is 93 mV.



In field tests a threshold value of the d.c. current density at 1 A/m² is empirically determined. The question rises regarding its significance. Based on Fig. 6 it is clear that the potential is limited by the hydrogen evolution. However, at increased current density it is possible to further decrease the potential of the steel surface according to Fig. 7. According to the model concept described in Fig 5 the electrochemical reduction of the passive film is the main reason for the occurrence of a.c. corrosion. According to the Pourbaix diagram the dissolution of the passive film is thermodynamically possible at potentials in the active range based on reaction (6). The potential difference between the equilibrium potential for hydrogen evolution and the equilibrium line between immunity and passivity is approximately 800 mV. Hence, a cathodic current that causes a potential shift of the steel surface of 800 mV is capable of destroying the passive film and, therefore, cause a.c. corrosion.

excursions. The main difference is the frequency of the interference. Using the data it could be assumed that similar mechanisms should take place during d.c. interference. Generally, an anodic interference is considered to be dangerous from the point of view of corrosion. However, comparing the polarization scans in Fig. 8 it becomes clear that similar behavior is obtained both at pH 8.4 and 12. In contrast, at pH 7 no passivity is observed. It is interesting to note that the onset of the anodic current is at -0.85 V CSE and at elevated potentials an increase in current is observed for the passive system. This increase corresponds to oxygen evolution. Based on this result it can be concluded that cathodic polarization primarily results in the formation of a passive film rather than corrosion. Anodic polarization even to significant potentials does not initiate any corrosion. From these data it could be concluded that anodic currents do not adversely affect the cathodic process of steel under cathodic protection. This is true as long as the pH value is high. This should be true if the off potential is more negative than -1 V CSE. If the off potential is cathodic current causes the pH to decrease. Some anodic reactions strongly depend on the pH. This is especially true for oxygen evolution that takes place at increased potentials. As decreasing pH the conditions for passivity can be lost and corrosion can be initiated. In consequence, the anodic current may only occur temporarily and the average current density through the steel surface must be cathodic in order to assure a sufficiently high pH. In the case of a.c. corrosion the repeated formation and dissolution of the passive film results in a high corrosion rate according to Fig. 5. The same process takes place in the case of d.c. interference. However, the lower frequency is strongly limiting the corrosion rate. The repeated formation and dissolution of the passive layer results in the formation of a porous layer, the amount of charge that can be consumed during the anodic excursions is significantly increased. This is due to reaction (5) that can consume major amounts of electrical charge without causing corrosion. This effect is reported by [2] for d.c. interference.

Fig. 8: Polarization scans of steel in various electrolytes.

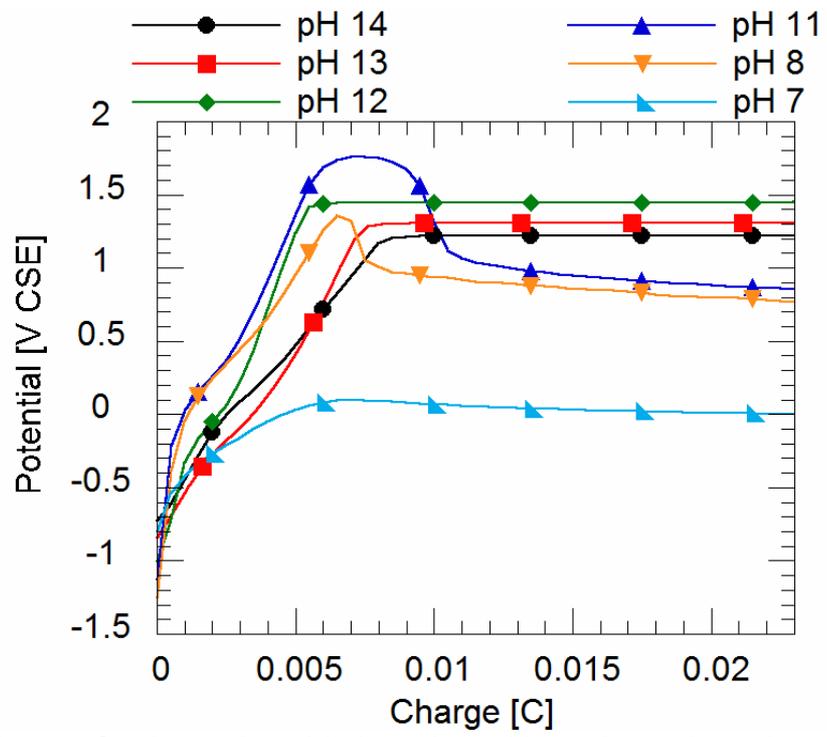


Fig. 9: Coulometric oxidation of steel in various electrolytes. The potential values are corrected for ohmic potential drop.

Fig. 10: Coulometric oxidation of an interred coupon after 12 years in service. *values are determined after short interruption of the current.*

Based on this discussion it becomes clear that anodic charge and anodic excursions do not necessarily cause corrosion. Therefore, neither a potential nor a charge criterion is necessarily applicable for judging the risk of stray current corrosion. As a consequence, the currently used criteria according to EN 50162 are clearly conservative. The risk of stray current corrosion is probably often overestimated.

A possible approach to the judging of the corrosion risk due to stray current is the use of the coulometric oxidation [5, 7]. By applying an anodic current on a steel coupon, the potential evolution can be determined over time. An example is shown in Fig. 9 for different electrolytes. Based on these data it is clear that oxygen evolution can only be prevented if the pH is sufficiently high to promote the formation of a protective passive film. The corrosion risk can be followed by the increase of potential, while the oxygen evolution results in a constant independent potential value above 0.5 V CSE. Once the oxygen evolution is reached, the potential starts decreasing which can cause initiation of corrosion. The corrosion initiation can be detected by the drop of potential as demonstrated for pH 11 and 8. In the case of pH 7, no passivation is observed at all since the potential does not rise up to oxygen evolution. From this short experiment the passivating properties of the soil in the vicinity of the pipeline can be judged.

If repeated formation and dissolution of a passive film has taken place, a rust layer can accumulate on the steel surface. This rust layer can significantly increase the anodic charge that can be consumed during anodic polarization. In Fig. 10 an example is shown on a coupon connected to a pipeline. A similar behavior as in Fig. 9 is observed. However, there is a larger amount of charge being consumed before oxygen evolution is reached. This can be attributed to the oxidation of the rust layer according to reaction (5).

Conclusion

The processes taking place under cathodic protection of steel are discussed in detail. On this analysis it has to be concluded that the corrosion protection is not achieved by the polarization of the steel surface to the immunity range. Instead the positive effect

The coulometric oxidation, which was developed for investigating the a.c. suggested as a technique for characterizing the resistance of coupons to potential excursions and judge the corrosion risk of the pipeline under interference.

Acknowledgements

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